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(51) International Patent Classification: **H01M 8/00** (74) Agent: **CHARIG, Raymond, J.**; Eric Potter Clarkson, Park View House, 58 The Ropewalk, Nottingham NG1 5DD (GB).

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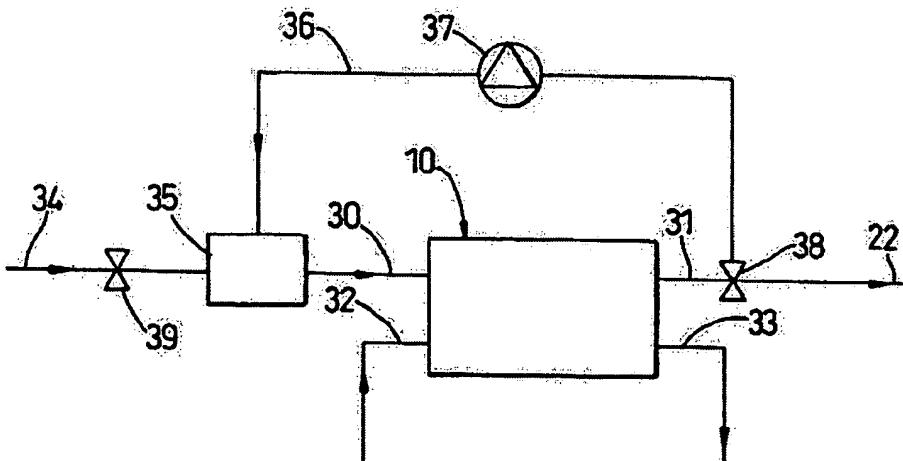
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(75) Inventors/Applicants (for US only): **MITCHELL, Philip, John** [GB/GB]; Intelligent Energy, 42 Brook Street, Mayfair, London W1K 5DB (GB). **ADCOCK, Paul, Leonard** [GB/GB]; Intelligent Energy, 42 Brook Street, Mayfair, London W1K 5DB (GB).

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(54) Title: **FUEL CELL OXYGEN REMOVAL AND PRE-CONDITIONING SYSTEM**



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(57) Abstract: A fuel cell having an anode, a cathode and an ion exchange membrane is supplied by hydrogen fuel through an anode fuel delivery conduit. A recirculation loop is provided to recycle gases in the fuel delivery conduit to a mixing point where a controlled flow rate of fuel is supplied and mixed therewith. Any oxidant species remaining in the fuel delivery conduit are thereby combusted in a controlled manner to avoid damage to the fuel cell membrane-electrode assembly. Small quantities of oxidant may be deliberately introduced into the fuel delivery conduit to generate water vapour and heat to pre-condition the fuel delivered to the anode. Such preconditioning assists in hydration control of the membrane, and temperature control of the membrane-electrode assembly for optimum fuel cell performance.



*For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.*

## FUEL CELL OXYGEN REMOVAL AND PRE-CONDITIONING SYSTEM

The present invention relates to fuel cells, and in particular to methods and  
5 apparatus for controllably removing oxidants in a fuel cell fuel supply  
stream.

Conventional electrochemical fuel cells convert fuel and oxidant into  
electrical energy and a reaction product. A typical layout of a conventional  
10 fuel cell 10 is shown in figure 1 which, for clarity, illustrates the various  
layers in exploded form. A solid polymer ion transfer membrane 11 is  
sandwiched between an anode 12 and a cathode 13. The polymer membrane  
allows protons to traverse the membrane, but blocks the passage of  
15 electrons. Typically, the anode 12 and the cathode 13 are both formed from  
an electrically conductive, porous material such as porous carbon, to which  
small particles of platinum and/or other precious metal catalyst are bonded.  
The anode 12 and cathode 13 are often bonded directly to the respective  
adjacent surfaces of the membrane 11. This combination is commonly  
20 referred to as the membrane-electrode assembly, or MEA.

Sandwiching the polymer membrane and porous electrode layers is an anode  
fluid flow field plate 14 and a cathode fluid flow field plate 15. The fluid  
flow field plates 14, 15 are formed from an electrically conductive, non-  
porous material by which electrical contact can be made to the respective  
25 anode electrode 12 or cathode electrode 13. At the same time, the fluid flow  
field plates must enable the delivery and/or exhaust of fluid fuel, oxidant  
and/or reaction products (and/or other diluent gases not taking part in the  
reaction) to or from the porous electrodes. This is conventionally effected  
by forming fluid flow passages in a surface of the fluid flow field plates,

such as grooves or channels 16 in the surface presented to the porous electrodes.

Figure 2 shows a plan view of a typical fluid flow channel 16 arranged as a 5 serpentine structure 20 in a face of the anode 14 (or cathode) having an inlet manifold 21 and an outlet manifold 22. Many different configurations of fluid flow channel may be used.

In a typical application, in the anode fluid flow field plate 14, hydrogen gas 10 is delivered into the serpentine channel 20 from the inlet manifold 21. In the cathode fluid flow field plate 15, oxidant (eg. oxygen gas) is delivered into the serpentine channel 20 from the inlet manifold.

Prior to the start up of a fuel cell 10 after first assembly, commissioning, 15 repair, prolonged periods of inactivity or stand-by there can be an accumulation of air in the fuel flow channels and fuel delivery conduits, ie. generally within the fuel delivery path of the fuel cell. There is therefore a need to remove this air, or more particularly to remove the oxygen in the air, from the anode fuel delivery path before the introduction of any hydrogen 20 fuel or a hydrogen rich gas mixture to the anode 12 and membrane 11.

This removal of oxygen prior to delivery of fuel is important to prevent undesirable uncontrolled catalytic combustion occurring at the surface of the anode 14 resulting in localized heating, dehydration and possible puncture of 25 the proton exchange membrane 11.

In the prior art, it is common practice to purge the anode channels 16 and other portions of the fuel delivery conduits by passage of an inert gas, such as nitrogen, for a period of time prior to introduction of hydrogen fuel.

This process necessitates a local supply of nitrogen, generally contained in a pressure cylinder, and its periodic replacement. It is desirable to eliminate this requirement and thereby simplify the operational and service needs of the system. This is particularly important when the fuel cell is already 5 installed in the field, eg. as part of a power system in a vehicle where accessibility of a purge gas, and indeed accessibility to the fuel cell, may be limited.

It is an object of the present invention to provide a convenient method and 10 apparatus for the removal of oxygen from the fuel delivery conduits of an electrochemical fuel cell.

It is a further object of the present invention to provide an apparatus by 15 which the removal of oxygen from the fuel delivery conduits of an electrochemical fuel cell may be effected automatically.

A further problem associated with start up of fuel cells is that the membrane-electrode assembly generally operates with optimum performance only once it has reached an ideal operating temperature and an ideal degree of 20 hydration of the membrane. Conventionally, such an optimum performance level is not achieved until after a period of operation of the fuel cell.

It is a further object of the invention to provide an apparatus by which a fuel 25 and/or oxidant gas stream is pre-conditioned to accelerate hydration of the membrane-electrode assembly and/or to accelerate heating of the membrane-electrode assembly towards an optimum operating condition.

According to one aspect, the present invention provides a fuel cell including an anode, a cathode, and an ion exchange membrane therebetween, and 30 having a fuel delivery conduit for supplying fuel from a fuel source to an

active surface area of the anode and further comprising means for effecting a controlled combustion of fuel and oxidant species within the fuel delivery conduit.

5 According to a further aspect, the present invention provides a fuel cell system including:

a fuel cell having an anode, a cathode, and an ion exchange membrane therebetween;

a fuel delivery conduit comprising:

10 a fluid flow field plate forming part of the anode, having a fluid flow channel extending therethrough;

a fuel delivery inlet coupled to one end of the fluid flow channel; and

15 a fuel delivery outlet coupled another end of the fluid flow channel;

the fuel cell system further comprising:

a recirculation conduit extending between the fuel delivery outlet and a mixing point in the fuel delivery inlet.

20 According to a further aspect, the present invention provides a fuel cell system including:

a fuel cell having an anode, a cathode, and an ion exchange membrane therebetween;

25 a fuel delivery conduit for delivering preconditioned fuel to the anode comprising:

a reaction chamber for reacting fuel and oxidant;

a fuel supply inlet for delivering fuel to the reaction chamber;

an oxidant supply inlet for supplying oxidant to the reaction chamber; and

30 a reaction chamber outlet connected to the anode;

the reaction chamber being adapted so that at least a part of the fuel supply delivered thereto to is reacted with the oxidant supplied thereto to precondition the fuel being delivered to the anode.

5 According to a further aspect, the present invention provides a fuel cell system including:

a fuel cell having an anode, a cathode, and an ion exchange membrane therebetween;

an oxidant delivery conduit for delivering preconditioned oxidant to  
10 the cathode comprising:

a reaction chamber for reacting fuel and oxidant;

a fuel supply inlet for delivering fuel to the reaction chamber;

an oxidant supply inlet for supplying oxidant to the reaction chamber; and

15 a reaction chamber outlet connected to the cathode;

the reaction chamber being adapted so that at least a part of the oxidant supply delivered thereto to is reacted with the fuel supplied thereto to precondition the oxidant being delivered to the cathode.

20 According to a further aspect, the present invention provides a method of operating a fuel cell having an anode, a cathode, and an ion exchange membrane therebetween, comprising the steps of:

supplying fuel from a fuel source to an active surface area of the anode by way of a fuel delivery conduit; and

25 effecting a controlled combustion of fuel and oxidant species within the fuel delivery conduit.

According to a further aspect, the present invention provides a method of operating a fuel cell having an anode, a cathode, and an ion exchange

30 membrane therebetween, comprising the steps of:

supplying fuel from a fuel source to an active surface area of the anode by way of a fuel delivery conduit; and

reacting fuel and oxidant in a reaction chamber upstream of the anode to precondition the fuel being delivered to the anode.

5

Embodiments of the present invention will now be described by way of example and with reference to the accompanying drawings in which:

Figure 1 is an exploded cross-sectional view of a prior art fuel cell;

Figure 2 is a plan view of a fluid flow field plate in the fuel cell of 10 figure 1;

Figure 3 is a schematic diagram of a first arrangement of an oxygen removal system according to the present invention;

Figure 4 is a schematic diagram of a second arrangement of an oxygen removal system according to the present invention;

15 Figure 5 is a schematic diagram of a preconditioning system for controlled combustion of fuel and oxidant in a fuel delivery conduit according to the present invention; and

Figure 6 is a schematic diagram of a further preconditioning system for controlled combustion of fuel and oxidant in a fuel delivery conduit 20 according to the present invention.

One method of achieving oxygen removal from the fuel delivery path is to utilize the oxygen in a controlled catalytic combustion of hydrogen external to the fuel cell.

25

With reference to figure 3, a fuel cell 10 is coupled to fuel delivery conduits 30, 31 and oxidant / exhaust conduits 32, 33. The fuel delivery conduits 30, 31 respectively provide an inlet 30 and outlet 31 for delivery to and from the anode fluid flow field plate 14 (figure 1) while the oxidant supply conduit 32 provides a supply of the oxidant to an inlet end of the cathode fluid flow

field plate 15 and the exhaust conduit 33 provides an outlet to exhaust unused oxidant and reaction products from the cathode.

5 A fuel supply (eg. hydrogen) is coupled to a system inlet 34 which is fed to a reaction chamber 35. A recycle loop 36 extends between outlet 31 and the reaction chamber. The recycle loop 36 incorporates a pump 37 and can be switched into operation using a two way valve 38.

10 The reaction chamber 35 contains a suitable catalytic material dispersed on a support, to enable the removal of oxidants passing therethrough, according to techniques well known in the art. Presently preferred catalytic materials include precious metals such as platinum or platinum alloys dispersed on a ceramic support such as alumina.

15 In a normal mode of use, a hydrogen fuel supply is provided to the fuel cell 10 by way of system inlet 34, preferably via a flow regulator or metering valve 39. The hydrogen fuel passes into the inlet manifold 21 and anode fluid flow field plate 14 (figure 1) where it is at least partially consumed. Any unconsumed fuel or inert diluent fluid in the fuel supply may be 20 exhausted via a fuel system outlet 22, when the two way valve 38 is switched to an exhaust position.

25 When the anode (fuel) stream is determined to be contaminated, or when it is suspected to be contaminated, by oxidant fluid, the system is switched to a recirculation mode of use. In this configuration, the two way valve 38 is switched so that the fuel cell outlet 31 is connected to the recycle loop 36. If necessary to maintain fluid circulation, the recycle pump 37 is switched on. In this manner, the anode fluid stream is recirculated, passing through reaction chamber 35 where oxidant species are scrubbed from the fluid

stream, preferably by reaction with a controlled bleed of hydrogen gas from fuel system inlet 34 and flow regulator 39.

5 In this manner, combustion of hydrogen and oxidant species is effected only in the reaction chamber 35 and not in the fuel cell 10.

The recirculation mode of use may be initiated according to any desired prevailing condition. These conditions may include any one or more of the following: (i) automatic detection of oxidant in the fuel delivery conduit 10 inlet 30 and/or outlet 31 by means of an appropriate sensor mechanism (to be described later); (ii) automatic detection of a period of non-use of the fuel cell exceeding a predetermined elapsed time threshold; (iii) automatic detection of a period of use of the fuel cell exceeding a predetermined elapsed time threshold; (iv) automatic detection of a service condition, ie. 15 after detection of a fuel cell maintenance condition; and (v) manual initiation, by a user.

During the recirculation mode, the gases in the fuel cell can be recirculated around the recycle loop 36 and through the reaction chamber 35 into which 20 the hydrogen gas is being introduced in a controlled manner, until all of the unwanted oxygen is eliminated. This recirculation mode may continue automatically for a predetermined period of time, or may be continued automatically until detection of reduction of unwanted oxidant species to below a predetermined threshold. Alternatively, the duration of the 25 recirculation mode may be controlled manually by the user.

The metered supply of hydrogen fuel from the flow regulator 39 ensures that combustion of the fuel and oxidant is restricted to the volume of the reaction chamber 35 and that no combustion takes place within the fuel cell itself.

The presence of an oxidant species in the fuel delivery conduits and in the anode conduits may be detected by a number of methods. A low, near zero, open circuit voltage of the fuel cell stack 10 is often a good indicator of the presence of oxygen on the anode electrode face. Once this oxygen has been 5 substantially removed, then the hydrogen will break through the reaction bed and transfer to the fuel cell anode surface thereby elevating the open circuit voltage and indicating successful oxygen elimination.

Thus, in one presently preferred embodiment, prior to operation of the fuel 10 cell, the open circuit voltage is tested. If this open circuit voltage is lower than a predetermined threshold, the system determines that a recirculation mode of operation using a low flow hydrogen supply should be initiated prior to entering normal operating mode. In a further embodiment, the open circuit voltage is continuously monitored during the recirculation mode until 15 the open circuit voltage exceeds a predetermined threshold.

In a further embodiment, the oxygen level may be detected by monitoring the temperature of the reaction chamber, or outlet thereof, using an appropriate thermocouple or thermistor. During the period when oxygen is 20 being reacted with fuel in the reaction chamber, the temperature of the reaction chamber, or of the gas flow exiting the reaction chamber, will continue to rise. Once the temperature rise ceases, begins to fall or slows below a predetermined rate of increase, it can be determined that the oxygen level has reduced to below an appropriate threshold indicating that the fuel 25 cell may be brought into normal operating mode.

Once the oxygen has been removed, the hydrogen flow rates can be increased to such levels as are consistent with normal power delivery from the fuel cell and normal operation can begin.

With reference to figure 4, an alternative method of achieving oxygen removal from the fuel delivery path is to utilize the oxygen in a controlled combustion of hydrogen internally of the fuel cell.

- 5 In this embodiment, the reaction chamber 35 is removed and the recycle loop 36 delivers the recirculated gas stream to a mixing point 40 where it is mixed with the controlled low flow bleed of hydrogen fuel from fuel system inlet 34 and flow regulator 39.
- 10 Preferably, the mixing point 40 comprises a pre-mixing chamber 41 incorporating a plurality of mixing baffles or other suitable physical structure to encourage a thorough mixing of fuel fluid with recirculation fluid prior to entry into the fuel cell. In this manner, a very controlled, low level reaction can be effected at the anode of the fuel cell in such a manner
- 15 as to avoid any significant level of damage to the fuel cell.

This relies on the catalytic activity at the anode surface in the fuel cell 10 to promote the reaction of fuel and oxidant in situ. Provided that close control of hydrogen dosing is observed and good pre-mixing before entry into the

- 20 fuel cell occurs, then localized heating effects within the anode will be avoided and good reaction distribution will occur avoiding damage to the fuel cell.

The metered hydrogen fuel may comprise a hydrogen rich gas, for example,

- 25 a hydrogen and inert diluent fluid mixture, offering further improvement in fuel and oxidant mixing.

Similar to the embodiment of figure 3, automatic control means may be provided for determining when the recirculation mode is to be initiated, and

- 30 for how long, prior to switching to a normal mode of operation.

A further aspect of preventing or limiting damage to the membrane-electrode assembly is to ensure that fuel delivered to the anode is provided at an optimum temperature and/or humidity. During a start up phase, control 5 of the temperature and/or humidity of the fuel stream can also accelerate the process of achieving an optimum operating condition in the fuel cell.

With reference now to figure 5, an adaptation of the process described in connection with figure 3 can be made to pre-condition the fuel flow by 10 introducing water or steam to improve or maintain humidity in the fuel gas stream. A further benefit of this arrangement is that the temperature of the fuel stream can also be controlled.

To achieve this fuel pre-conditioning, provision is made to deliver oxidant 15 (eg. air) into the reaction chamber 35 to deliberately increase the reaction of hydrogen with oxygen for the purpose of producing water and heat.

An oxidant supply line 50 is connected to supply of suitable oxidant. In the preferred embodiment shown, this supply is conveniently the same source of 20 oxidant used to supply the cathode, namely the oxidant supply conduit 32. The oxidant supply line 50 is coupled thereto by a valve 51, which may also incorporate a flow regulator (not shown separately). This system configuration may be used with or without the recycle loop 36 depicted in figures 3 and 4.

25

The provision of controlled quantities of oxidant to the reaction chamber 35 results in a predetermined rate of reaction of hydrogen and oxygen in the reaction chamber, thereby enabling control of the temperature and humidity of the fuel gas being fed to the fuel cell 10 anode via fuel delivery conduit

inlet 30 (assuming, of course, that the fuel supply from flow regulator 39 provides excess fuel to that required by the oxidant supply).

The flow of water or water vapour to the fuel cell 10 (and its continued re-circulation if used in combination with the recycle loop 36) allows the hydration state of the membrane to be controlled hence maintaining conductivity by use of a pre-conditioned fuel stream.

This facility is particularly useful in the operation of fuel cells of open cathode design, which are prone to membrane dehydration when not operated for extended periods of time.

Energy is liberated in the course of the reaction in reaction chamber 35 and therefore offers the opportunity to deliver heat directly to the fuel cell or any other part of the associated system by means of heat exchange / transfer mechanisms. This may be of particular use when starting a fuel cell from cold where the rapid elevation of temperature will ensure a shorter time to normal operational temperature and maximum power capability.

20 In any case the use of a catalytic reactor, upstream of fuel gas introduction and /or in a recirculation loop provides the additional flexibility of controlling fuel gas humidity and introducing heat via the gas stream.

25 With reference to figure 6, a further arrangement is shown that allows for provision of humidification and pre-heating of both the fuel flow to the anode of the fuel cell 10, and separate humidification and pre-heating of oxidant flow to the cathode of the fuel cell 10.

30 In this arrangement, the fuel system inlet 34 is coupled to feed a first reaction chamber 35 within the fuel delivery conduit 30, which is supplied

by an oxidant supply line 50. The oxidant supply conduit 32 incorporates a second reaction chamber 60 which is supplied by a fuel supply line 61. Appropriate valves 62, 63 control the flow of oxidant and fuel to respective first and second reaction chambers 35, 60, which valves may also include 5 flow regulators for varying flow rate according to a desired degree of humidification and/or pre-heat.

It will be understood that either or both of the first and second reaction chambers could be used independently of the other. In addition, the system 10 of figure 6 could also be used in conjunction with a recycle loop as described in connection with figure 3.

The preconditioning mode of operation described in connection with figures 5 and 6 may be initiated according to any desired prevailing condition. 15 These conditions may include any one or more of the following: (i) automatic detection of a period of non-use of the fuel cell exceeding a predetermined elapsed time threshold; (ii) automatic detection of a period of use of the fuel cell exceeding a predetermined elapsed time threshold; (iii) automatic detection of a service condition, ie. after detection of a fuel cell 20 maintenance condition; (iv) automatic detection of a predetermined temperature or humidity condition in the fuel delivery conduit or fuel cell, and (v) manual initiation, by a user.

The preconditioning mode of operation may continue automatically for a 25 predetermined period of time, indefinitely, or may be continued automatically until detection of a suitable temperature or humidity condition in the fuel delivery conduit or fuel cell. Alternatively, the duration of the preconditioning mode may be controlled manually by the user.

Throughout the present specification, for convenience the fuel cell 10 has been described in terms of only a single anode, membrane and cathode. However, it will be understood that, in accordance with conventional fuel cell design, multiple membrane-electrode assemblies are used in series or in 5 parallel in a stack in order to increase the voltage and/or current supply. In accordance therewith, the fuel delivery conduit typically incorporates a plurality of anode fluid flow field plates, and the oxidant supply conduit typically incorporates a plurality of cathode fluid flow field plates. The principles of the present invention apply equally to such membrane-10 electrode assembly stacks.

The invention has been described with reference to a conventional MEA comprising a polymer membrane, but is also relevant to other types of fuel cell.

15

Other embodiments are within the accompanying claims.

**CLAIMS**

1. A fuel cell including an anode, a cathode, and an ion exchange membrane therebetween, and having a fuel delivery conduit for supplying fuel from a fuel source to an active surface area of the anode and further comprising means for effecting a controlled combustion of fuel and oxidant species within the fuel delivery conduit.
2. A fuel cell according to claim 1 in which the fuel delivery conduit comprises a fluid flow field plate forming part of the anode, having a fluid flow channel extending therethrough; a fuel delivery inlet coupled to one end of the fluid flow channel; and a fuel delivery outlet coupled another end of the fluid flow channel.
3. A fuel cell according to claim 2 in which the means for effecting a controlled combustion of fuel and oxidant species within the fuel delivery conduit comprises:
  - a recirculation conduit extending between the fuel delivery outlet and a mixing point in the fuel delivery inlet, and
  - 20 a fluid flow regulator for controllably varying the quantity of fuel delivered to the mixing point.
4. A fuel cell according to claim 3 in which the mixing point comprises a reaction chamber for reacting fuel from said fluid flow regulator with oxidant species from said recirculation conduit.
5. A fuel cell according to claim 4 in which the reaction chamber includes a catalyst material.

6. A fuel cell according to claim 3 in which the mixing point comprises a pre-mixing chamber for mixing fuel from said fluid flow regulator with oxidant species from said recirculation conduit.
- 5 7. A fuel cell according to any preceding claim in which the recirculation conduit is switchably connected to the fuel delivery outlet by way of a two way valve.
- 10 8. A fuel cell according to any preceding claim further including detection means for detecting a level of oxidant species present in at least part of the fuel delivery conduit.
- 15 9. A fuel cell according to claim 8 in which the detection means comprises means for testing an open circuit voltage across the anode and cathode of the fuel cell.
- 20 10. A fuel cell according to claim 3 further including control means for switching the fuel cell between a normal mode of operation in which a relatively high flow rate of fuel is delivered to the anode and oxidant is delivered to the cathode, and a recirculation mode in which a relatively low flow rate of fuel is delivered to the anode together with oxidant delivered via the recirculation conduit.
- 25 11. A fuel cell according to claim 3 further including control means for switching the fuel cell between a normal mode of operation in which a relatively high flow rate of fuel is delivered to the anode and oxidant is delivered to the cathode, and a recirculation mode in which a relatively low flow rate of fuel is delivered into fuel delivery conduit together with oxidant delivered via the recirculation conduit.

12. A fuel cell according to claim 2 in which the means for effecting a controlled combustion of fuel and oxidant species within the fuel delivery conduit comprises an oxidant supply conduit extending from an oxidant supply to a mixing point in the fuel delivery inlet.

5

13. A fuel cell according to claim 12 further including an oxidant flow regulator for controllably varying the quantity of oxidant delivered to the mixing point.

10 14. A fuel cell according to claim 13 in which the oxidant flow regulator comprises a valve coupling the oxidant supply conduit to a cathode oxidant delivery conduit.

15. A fuel cell according to claim 12 in which the mixing point comprises a reaction chamber for reacting fuel from said fluid flow regulator with oxidant species from said oxidant supply conduit.

16. A fuel cell according to claim 15 in which the reaction chamber includes a catalyst material.

20

17. A fuel cell according to claim 1 further including means for effecting a controlled combustion of fuel and oxidant species within a cathode fluid delivery conduit.

25 18. A fuel cell according to claim 17 in which the cathode fluid delivery conduit comprises a fluid flow field plate forming part of the cathode, having a fluid flow channel extending therethrough; an oxidant delivery inlet coupled to one end of the cathode fluid flow channel; and an exhaust outlet coupled to another end of the cathode fluid flow channel.

30

19. A fuel cell according to claim 18 in which said means for effecting a controlled combustion within a cathode comprises a fuel supply conduit extending from an fuel supply to a mixing point in the oxidant delivery inlet.

5 20. A fuel cell according to claim 19 in which the mixing point comprises a reaction chamber for reacting fuel from said fuel supply conduit with oxidant species from said oxidant supply.

21. A fuel cell system including:

10 a fuel cell having an anode, a cathode, and an ion exchange membrane therebetween;

a fuel delivery conduit comprising:

a fluid flow field plate forming part of the anode, having a fluid flow channel extending therethrough;

15 a fuel delivery inlet coupled to one end of the fluid flow channel; and

a fuel delivery outlet coupled another end of the fluid flow channel;

the fuel cell system further comprising

20 a recirculation conduit extending between the fuel delivery outlet and a mixing point in the fuel delivery inlet.

22. A fuel cell system according to claim 21 further including a fluid flow regulator for controllably varying the quantity of fuel delivered to the

25 mixing point.

23. A fuel cell system according to claim 21 or claim 22 in which the mixing point comprises a reaction chamber for reacting fuel from said fluid flow regulator with oxidant species from said recirculation conduit.

24. A fuel cell system according to claim 21 or claim 22 in which the mixing point comprises a pre-mixing chamber for mixing fuel from said fluid flow regulator with oxidant species from said recirculation conduit.

5 25. A fuel cell system according to claim 21 in which the recirculation conduit is switchably connected to the fuel delivery outlet by way of a two way valve.

10 26. A fuel cell system according to claim 21 further including detection means for detecting a level of oxidant species present in at least part of the fuel delivery conduit.

15 27. A fuel cell according to claim 26 in which the detection means comprises means for testing an open circuit voltage across the anode and cathode of the fuel cell.

20 28. A fuel cell system according to claim 21 further including control means for switching the fuel cell between a normal mode of operation in which a relatively high flow rate of fuel is delivered to the anode and oxidant is delivered to the cathode, and a recirculation mode in which a relatively low flow rate of fuel is delivered to the anode together with oxidant delivered via the recirculation conduit.

25 29. A fuel cell system according to claim 21 further including control means for switching the fuel cell between a normal mode of operation in which a relatively high flow rate of fuel is delivered to the anode and oxidant is delivered to the cathode, and a recirculation mode in which a relatively low flow rate of fuel is delivered into fuel delivery conduit together with oxidant delivered via the recirculation conduit.

30

30. A fuel cell system including:  
a fuel cell having an anode, a cathode, and an ion exchange membrane therebetween;  
a fuel delivery conduit for delivering preconditioned fuel to the anode  
5 comprising:  
a reaction chamber for reacting fuel and oxidant;  
a fuel supply inlet for delivering fuel to the reaction chamber;  
an oxidant supply inlet for supplying oxidant to the reaction chamber; and  
10 a reaction chamber outlet connected to the anode;  
the reaction chamber being adapted so that at least a part of the fuel supply delivered thereto is reacted with the oxidant supplied thereto to precondition the fuel being delivered to the anode.

15. 31. A fuel cell system according to claim 30 further including control means for controllably varying the flow rate of one or both of the fuel and oxidant in order to achieve a predetermined degree of humidification of the fuel stream delivered to the anode.

20. 32. A fuel cell system according to claim 30 further including control means for controllably varying the flow rate of one or both of the fuel and oxidant in order to achieve a predetermined degree of pre-heat of the fuel stream delivered to the anode.

25. 33. A fuel cell system including:  
a fuel cell having an anode, a cathode, and an ion exchange membrane therebetween;  
an oxidant delivery conduit for delivering preconditioned oxidant to the cathode comprising:  
30 a reaction chamber for reacting fuel and oxidant;

a fuel supply inlet for delivering fuel to the reaction chamber;  
an oxidant supply inlet for supplying oxidant to the reaction chamber; and

a reaction chamber outlet connected to the cathode;

5 the reaction chamber being adapted so that at least a part of the oxidant supply delivered thereto to is reacted with the fuel supplied thereto to precondition the oxidant being delivered to the cathode.

34. A fuel cell system according to claim 33 further including control  
10 means for controllably varying the flow rate of one or both of the fuel and  
oxidant in order to achieve a predetermined degree of humidification of the  
oxidant stream delivered to the cathode.

35. A fuel cell system according to claim 33 further including control  
15 means for controllably varying the flow rate of one or both of the fuel and  
oxidant in order to achieve a predetermined degree of pre-heat of the oxidant  
stream delivered to the cathode.

36. Apparatus substantially as described herein with reference to the  
20 accompanying drawings.

37. A method of operating a fuel cell having an anode, a cathode, and an  
ion exchange membrane therebetween, comprising the steps of:  
supplying fuel from a fuel source to an active surface area of the  
25 anode by way of a fuel delivery conduit; and  
effecting a controlled combustion of fuel and oxidant species within  
the fuel delivery conduit.

38. The method of claim 37 further including the step of recirculating fluid within the fluid delivery conduit to a mixing point upstream of the active surface area of the anode.

5 39. The method of claim 38 further including the step of consuming oxidant species at the mixing point, in a reaction chamber.

40. The method of claim 38 or claim 39 further including the step of controllably varying the quantity of fuel delivered to the mixing point.

10 41. The method of any one of claims 37 to 40 further including the step of detecting a level of oxidant species present in at least part of the fuel delivery conduit.

15 42. The method of claim 38 further including the steps of switching the fuel cell between a normal mode of operation in which a relatively high flow rate of fuel is delivered to the anode and oxidant is delivered to the cathode, and a recirculation mode in which a relatively low flow rate of fuel is delivered to the anode together with oxidant delivered in the recirculated fluid.

20 43. The method of claim 38 further including the steps of switching the fuel cell between a normal mode of operation in which a relatively high flow rate of fuel is delivered to the anode and oxidant is delivered to the cathode, and a recirculation mode in which a relatively low flow rate of fuel is delivered into the fuel delivery conduit together with oxidant delivered in the recirculation fluid.

25 44. A method of operating a fuel cell having an anode, a cathode, and an ion exchange membrane therebetween, comprising the steps of:

supplying fuel from a fuel source to an active surface area of the anode by way of a fuel delivery conduit; and

reacting fuel and oxidant in a reaction chamber upstream of the anode to precondition the fuel being delivered to the anode.

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45. The method of claim 44 further including the step of controlling the flow rate of one or both of the fuel and oxidant in order to achieve a predetermined degree of humidification of the fuel stream delivered to the anode.

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46. The method of claim 44 further including the step of controlling the flow rate of one or both of the fuel and oxidant in order to achieve a predetermined degree of pre-heat of the fuel stream delivered to the anode.

15

47. A method of operating a fuel cell having an anode, a cathode, and an ion exchange membrane therebetween, comprising the steps of:

supplying oxidant from an oxidant source to an active surface area of a cathode by way of an oxidant delivery conduit; and

20 reacting fuel and oxidant in a reaction chamber upstream of the cathode to precondition the oxidant being delivered to the cathode.

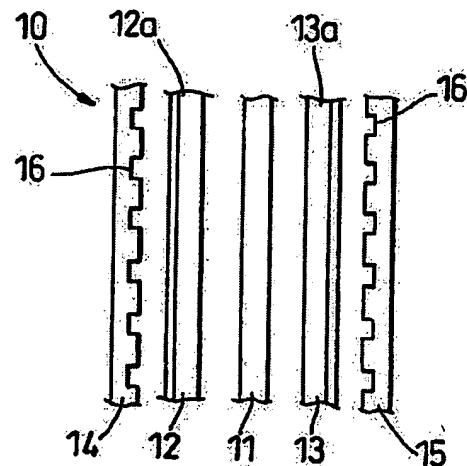
25

48. The method of claim 47 further including the step of controlling the flow rate of one or both of the fuel and oxidant in order to achieve a predetermined degree of humidification of the oxidant stream delivered to the cathode.

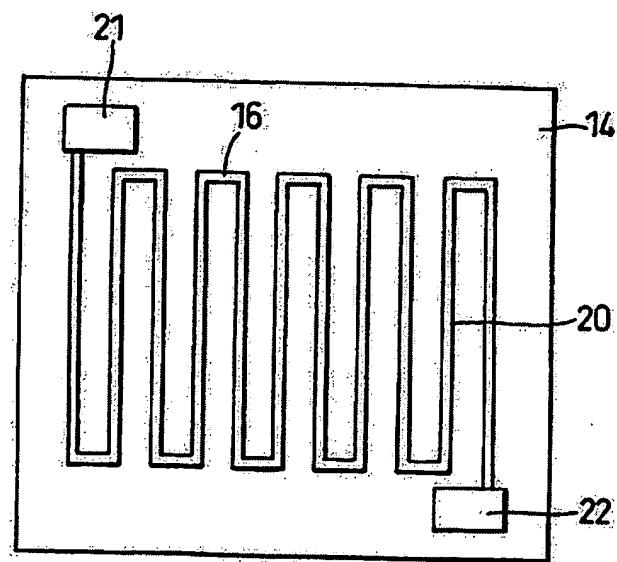
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49. The method of claim 47 further including the step of controlling the flow rate of one or both of the fuel and oxidant in order to achieve a predetermined degree of pre-heat of the oxidant stream delivered to the cathode.

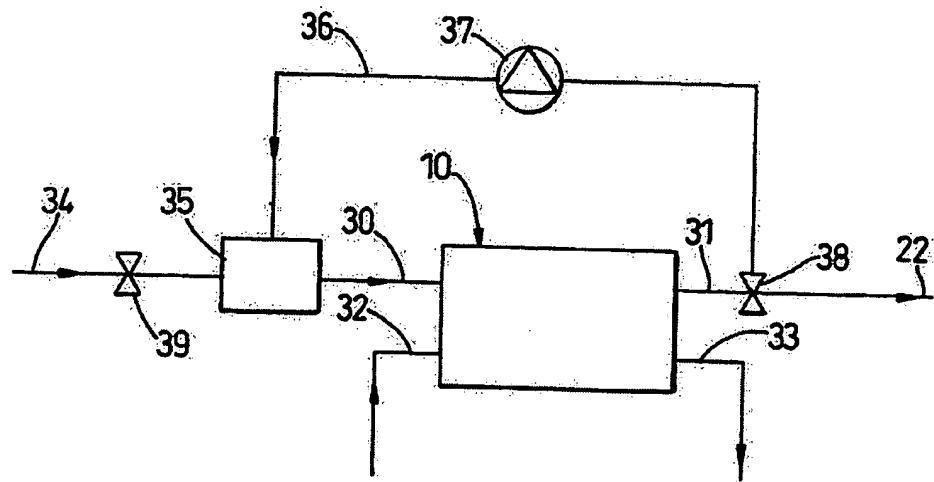
50. A method substantially as described herein with reference to the accompanying drawings.



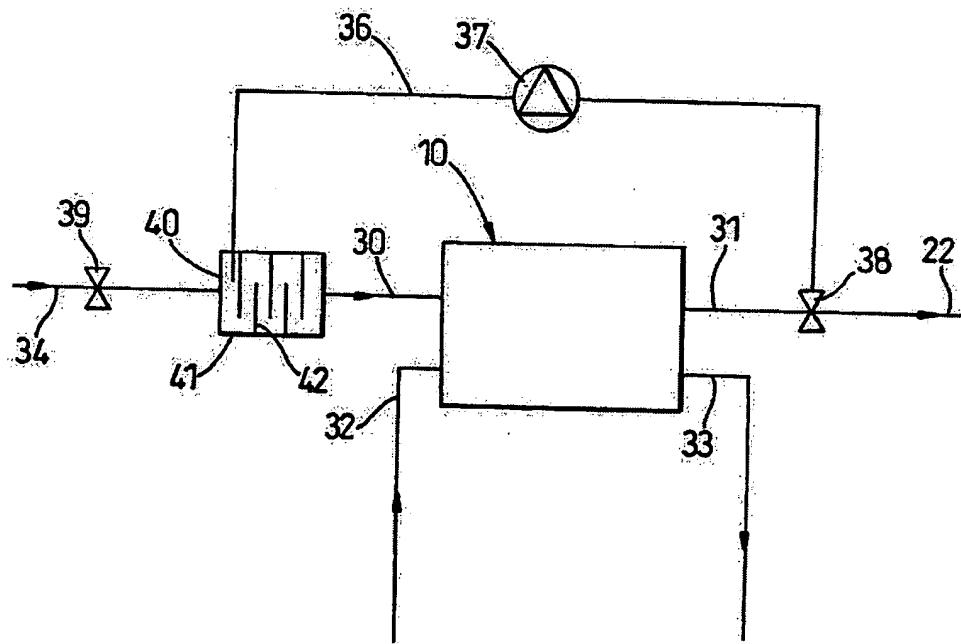
*Fig. 1*



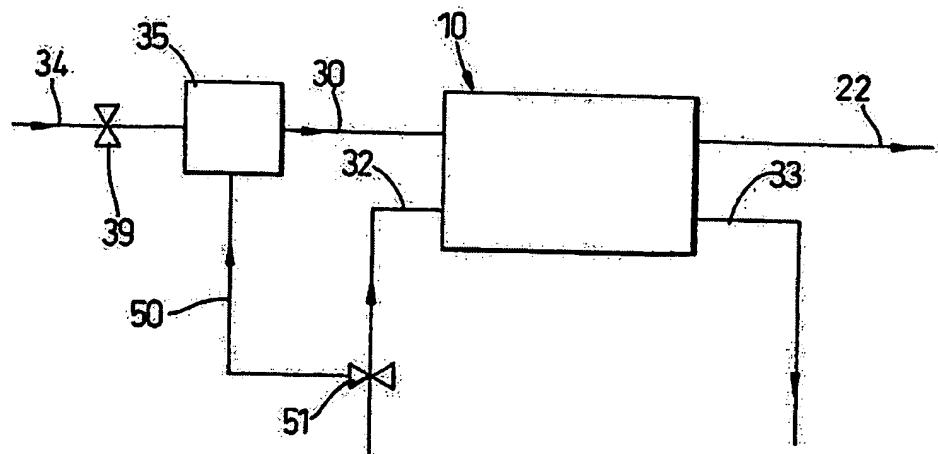
*Fig. 2*



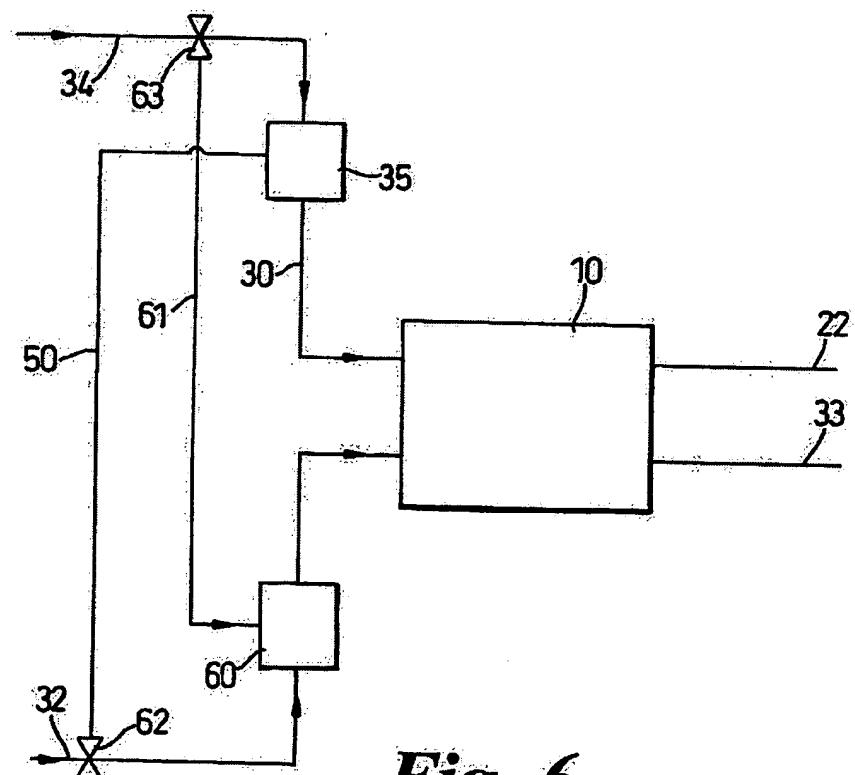
*Fig. 3*



*Fig. 4*



*Fig. 5*



*Fig. 6*

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(71) Applicant (for all designated States except US): INTELLIGENT ENERGY LIMITED [GB/GB]; Rolls House, 7 Rolls Buildings, Fetter Lane, London EC4A 1NH (GB).

(72) Inventors; and

(73) Inventors/Applicants (for US only): MITCHELL, Philip, John [GB/GB]; Intelligent Energy, 42 Brook Street, Mayfair, London W1K 5DB (GB); ADCOCK, Paul, Leonard [GB/GB]; Intelligent Energy, 42 Brook Street, Mayfair, London W1K 5DB (GB).

(74) Agent: CHARIG, Raymond, J.; Eric Potter Clarkson, Park View House, 58 The Ropewalk, Nottingham NG1 5DD (GB).

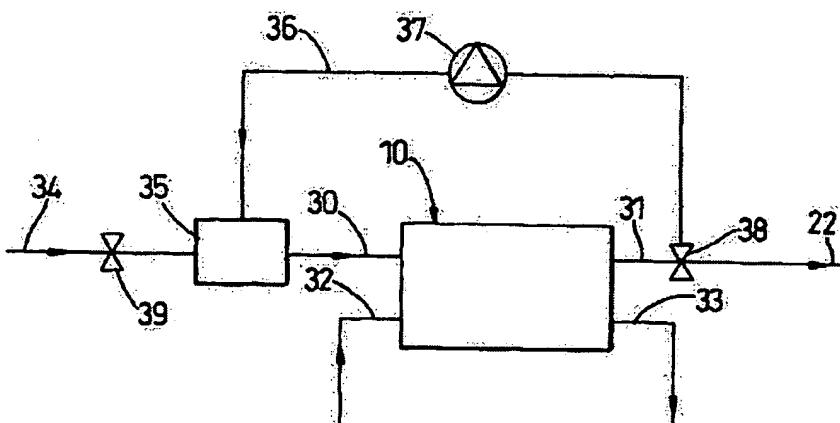
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Published:  
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(Continued on next page)

(54) Title: FUEL CELL OXYGEN REMOVAL AND PRE-CONDITIONING SYSTEM



WO 2003/063278 A3

(57) Abstract: A fuel cell having an anode, a cathode and an ion exchange membrane is supplied by hydrogen fuel through an anode fuel delivery conduit. A recirculation loop is provided to recycle gases in the fuel delivery conduit to a mixing point where a controlled flow rate of fuel is supplied and mixed therewith. Any oxidant species remaining in the fuel delivery conduit are thereby combusted in a controlled manner to avoid damage to the fuel cell membrane-electrode assembly. Small quantities of oxidant may be deliberately introduced into the fuel delivery conduit to generate water vapour and heat to pre-condition the fuel delivered to the anode. Such preconditioning assists in hydration control of the membrane, and temperature control of the membrane-electrode assembly for optimum fuel cell performance.



— before the expiration of the time limit for amending the claims and to be republished in the event of receipt of amendments

For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

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## INTERNATIONAL SEARCH REPORT

PCT/GB 03/00169

A. CLASSIFICATION OF SUBJECT MATTER  
 IPC 7 H01M8/04 H01M8/06

According to International Patent Classification (IPC) or to both national classification and IPC

## B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)  
 IPC 7 H01M

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the International search (name of data base and, where practical, search terms used)

EPO-Internal, WPI Data, PAJ

## C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
P, X	US 6 376 113 B1 (PLEDGER WILLIAM A. ET AL) 23 April 2002 (2002-04-23)  column 6, line 29 – line 58; claims 1-37; figures 4,5	1-7, 10-16, 21-25, 28-32, 37-46
X	WO 01/39310 A (INT FUEL CELLS LLC) 31 May 2001 (2001-05-31)  page 11 – page 15 page 16, line 30 – page 27, line 33; figures 1,3	1-7, 10-16, 21-25, 30-32, 37-46

 Further documents are listed in the continuation of box C. Patent family members are listed in annex.

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Date of the actual completion of the International search

7 October 2004

Date of mailing of the International search report

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European Patent Office, P.B. 6818 Patenttaan 2  
 NL - 2280 HV Rijswijk  
 Tel: (+31-70) 340-2040, Tx: 91 651 epo nl  
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## INTERNATIONAL SEARCH REPORT

PCT/GB 03/00169

C(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT		
Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	PATENT ABSTRACTS OF JAPAN vol. 0133, no. 71 (E-807), 17 August 1989 (1989-08-17) & JP 1 124962 A (FUJI ELECTRIC CO. LTD), 17 May 1989 (1989-05-17) abstract	1, 21, 30, 37, 44
X	PATENT ABSTRACTS OF JAPAN vol. 0174, no. 24 (E-1410), 6 August 1993 (1993-08-06) & JP 5 089899 A (HITACHI LTD), 9 April 1993 (1993-04-09) abstract	1, 21, 30, 37, 44
X	WO 01/97310 A (FRANK DAVID ; RIVARD PIERRE (CA); CHEN XUESONG (CA); CARNELLI JOSEPH) 20 December 2001 (2001-12-20)  page 8, line 20 – page 10, line 12; figures 1-3	1, 17-20, 26, 33-35, 47-49
A	US 6 007 931 A (VAN DINE LESLIE L ET AL) 28 December 1999 (1999-12-28) the whole document	1-35, 37-49

## INTERNATIONAL SEARCH REPORT

PCT/GB 03/00169

**Box 1 Observations where certain claims were found unsearchable (Continuation of Item 1 of first sheet)**

This International Search Report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:

1.  Claims Nos.: because they relate to subject matter not required to be searched by this Authority, namely:
  
2.  Claims Nos.: 36, 50 because they relate to parts of the International Application that do not comply with the prescribed requirements to such an extent that no meaningful International Search can be carried out, specifically:  
see FURTHER INFORMATION sheet PCT/ISA/210
  
3.  Claims Nos.: because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).

**Box II. Observations where unity of invention is lacking (Continuation of item 2 of first sheet)**

This International Searching Authority found multiple inventions in this international application, as follows:

1.  As all required additional search fees were timely paid by the applicant, this International Search Report covers all searchable claims.
2.  As all searchable claims could be searched without effort justifying an additional fee, this Authority did not invite payment of any additional fee.
3.  As only some of the required additional search fees were timely paid by the applicant, this International Search Report covers only those claims for which fees were paid; specifically claims Nos.:
4.  No required additional search fees were timely paid by the applicant. Consequently, this International Search Report is restricted to the invention first mentioned in the claims. It is covered by claims Nos.:

### Remark on Protest

The additional search fees were accompanied by the applicant's protest.

No protest accompanied the payment of additional search fees.

**FURTHER INFORMATION CONTINUED FROM PCT/ISA/ 210**

**Continuation of Box I.2**

**Claims Nos.:** 36, 50

Present claims 36 and 50 relate to an extremely large number of possible apparatus and methods. In fact, the claims contain so many options, variables, possible permutations and provisos that a lack of clarity (and conciseness) within the meaning of Article 6 PCT arises to such an extent as to render a meaningful search of the claims impossible.

The applicant's attention is drawn to the fact that claims relating to inventions in respect of which no international search report has been established need not be the subject of an international preliminary examination (Rule 66.1(e) PCT). The applicant is advised that the EPO policy when acting as an International Preliminary Examining Authority is normally not to carry out a preliminary examination on matter which has not been searched. This is the case irrespective of whether or not the claims are amended following receipt of the search report or during any Chapter II procedure. If the application proceeds into the regional phase before the EPO, the applicant is reminded that a search may be carried out during examination before the EPO (see EPO Guideline C-VI, 8.5), should the problems which led to the Article 17(2) declaration be overcome.

## INTERNATIONAL SEARCH REPORT

PCT/GB 03/00169

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